

# *Mechanistic study of Cl<sub>2</sub> evolution at Ti-supported Co<sub>3</sub>O<sub>4</sub> anodes\**

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Co<sub>3</sub>O<sub>4</sub> layers were prepared by thermal decomposition of Co(NO<sub>3</sub>)<sub>2</sub> at various temperatures in the range 200–500° C on a Ti support with and without an interlayer of RuO<sub>2</sub>. Kinetic studies were carried out with and without dissolved Cl<sub>2</sub> at various partial pressures in NaCl solutions of concentration in the range 0.5–5 mol dm<sup>-3</sup>. The effect of the solution pH was especially investigated. Kinetic measurements were carried out both close to and far from equilibrium. The following parameters were determined: transfer coefficient, Tafel slope, stoichiometric number, reaction orders with respect to Cl<sup>-</sup>, H<sup>+</sup> and surface sites, activation energy. The most intriguing feature observed was the retarding effect of acidity on the anodic Cl<sub>2</sub> reaction. This has been ascribed to the complex surface behaviour of oxides in solution. A detailed mechanistic scheme has been proposed and discussed. The stability of the oxide surface was monitored by measuring the voltammetric charge in alkaline solution after sets of experiments.

## 1. Introduction

Co<sub>3</sub>O<sub>4</sub> is an electrode material which arouses great interest in the chlor-alkali industry [1, 2] because of its good electrocatalytic properties, ready availability and low cost. Nevertheless, published studies of chlorine evolution at Co<sub>3</sub>O<sub>4</sub>-activated Ti anodes are scanty and no detailed mechanistic investigation has been reported thus far [3–6]. The aim of the present work has been to study the mechanism of chlorine evolution from concentrated brines and to elucidate the influence of the temperature of Co<sub>3</sub>O<sub>4</sub> formation and the effect of the solution pH.

## 2. Experimental

Square Ti plates of 1 cm<sup>2</sup> geometric surface and 0.5 mm thickness with a tiny stem in the middle of one of the sides were used as support. These were first sandblasted, then etched in boiling 20% HCl, rinsed with distilled water and wiped with filter paper. The preparation of the Co<sub>3</sub>O<sub>4</sub> layer

was carried out by thermal decomposition of Co(NO<sub>3</sub>)<sub>2</sub> · 6H<sub>2</sub>O in air at temperatures ranging from 200 to 500° C [7, 8]. A 0.2 mol dm<sup>-3</sup> solution of the cobalt salt in isopropanol was brushed onto the two faces of the support (immediately after pre-treatment) and the solvent evaporated at 30–40° C. Samples were then fired in a well-furnace at the selected temperature for 10 min. The deposition of additional layers was continued until the desired amount of Co<sub>3</sub>O<sub>4</sub> was deposited (about 1.8 mg cm<sup>-2</sup> corresponding to *c.* 3 μm nominal thickness of the coating). Finally, the samples were annealed for 2 h at the same temperature.

Two sets of electrodes were prepared. In one set Co<sub>3</sub>O<sub>4</sub> was deposited directly onto Ti. In the other set, a thin interlayer of RuO<sub>2</sub>, prepared at 400° C in the usual way [9], was placed between the Ti and the active layer of Co<sub>3</sub>O<sub>4</sub>. Layers were prepared at 200, 230, 260, 300, 400 and 500° C. Two samples were prepared at each temperature in each set (total of 24 electrodes). The physico-chemical characterization of films of Co<sub>3</sub>O<sub>4</sub> on Ti has been reported previously [8].

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Solutions for kinetic experiments were prepared volumetrically with double-distilled water. Chemicals (Merck) and gases (SIAD) were used without further purification. Potentials were measured against a saturated calomel electrode, except when  $\text{ClO}_4^-$  ions were present in solution. In that case, a saturated NaCl calomel electrode was used. Electrodes were placed in a cylindrical cell with a Luggin capillary (connected to the compartment of the reference electrode and coming up from the bottom of the cell) placed at about 1 mm from the lower edge of the plate electrode. Two platinized Pt counter-electrodes facing the two opposite sides of the plate were separated by glass frits from the main compartment. During experiments the solution was usually saturated with pure nitrogen or nitrogen-chlorine mixtures and stirred by a magnetic stirrer. All experiments were carried out at  $25 \pm 0.1^\circ \text{C}$  unless otherwise stated.

Voltammetric curves were normally recorded in  $1 \text{ mol dm}^{-3}$  KOH solutions at  $20 \text{ mV s}^{-1}$  over an anodic potential range of 600 mV starting from  $-110 \text{ mV}$  (SCE) corresponding to the average rest potential of  $\text{Co}_3\text{O}_4$  electrodes in the alkaline solution. Voltammetric curves were integrated up to the potential of incipient oxygen evolution and the total charge (anodic + cathodic), henceforth denoted by  $q^*$ , has been used as a parameter to characterize the 'electrochemically active' surface area. Details of the determination of  $q^*$  will be given in a forthcoming paper [10].

Experiments on chlorine evolution were carried out in  $0.5\text{--}5 \text{ mol dm}^{-3}$  NaCl solutions to which  $10^{-2} \text{ mol dm}^{-3}$  HCl was added to keep the pH low. The nominal pH of these solutions is *c.* 2 but the effect of the NaCl concentration on the pH value will be discussed later. Potentiostatic curves were started either at the equilibrium potential (in  $\text{Cl}_2$  saturated solutions) or at 900 mV (SCE) after a conditioning time of 10 min. The potential was then increased in 20 mV steps and the current was read after 3 min. These experiments were carried out with the aid of a 551 AMEL potentiostat-galvanostat coupled with a 566 AMEL function generator. Currents were either read with a Microva AL 4 Kipp-Zonen galvanometer or recorded with a 862/D AMEL X-Y recorder. Potentials were read either with a 667/RM AMEL electrometer or with a 8687 L&N potentiometer.

The pH of the solution was measured by means of a 335 AMEL digital pH meter equipped with combined electrodes. These were carefully calibrated before each run using fresh buffers.

Since the electrode surface may undergo modifications upon prolonged anodic polarization, reaction order measurements were carried out by polarizing the electrode only at the selected potential. Thus, the electrode was conditioned for 10 min at 0.9 V (SCE), the potential was then stepped to the selected value and the current read after 3 min. The electrode was then stepped back to the conditioning potential, kept there for 10 min and removed from the cell. This operation was repeated for each different concentration of the species under study.

### 3. Results and discussion

#### 3.1. Voltametric curves

Fig. 1 shows a comparison between the behaviour of  $\text{Co}_3\text{O}_4$  in the absence and in the presence of chloride ions. The voltametric curve in the blank solution does not show the typical current maxima related to the adsorption-desorption of oxygenated species [7, 10-12]. This is because this maximum, visible in KOH solutions prior to  $\text{O}_2$  evolution, shifts with pH at a greater rate than the anodic process itself [7, 11, 12].  $\text{Cl}_2$  evolution, at the same pH, commences about 140 mV earlier than  $\text{O}_2$  evolution. Both curves are featureless prior to the anodic reaction. The charging current is depressed by the presence of  $\text{Cl}^-$  ions in solution. This may be related to a lowering of the (pseudo) capacitance of the oxide-solution interface as a result of  $\text{Cl}^-$  adsorption. In fact, the surface of  $\text{Co}_3\text{O}_4$  at low pHs carries a strong positive charge [13].

#### 3.2. Equilibrium potential

Fig. 2 shows the dependence of the equilibrium potential of  $\text{Co}_3\text{O}_4$  electrodes on the  $\text{Cl}_2$  partial pressure and the  $\text{Cl}^-$  activity in solution. A strictly Nernstian behaviour is observed at variable  $p_{\text{Cl}_2}$ , and also at constant  $a_{\text{Cl}^-}$  in the low  $\text{Cl}_2$  pressure range. Small deviations are observed in the high  $p_{\text{Cl}_2}$  range as  $a_{\text{Cl}^-}$  is varied. The origin of these small deviations is not clear. Equilibrium poten-

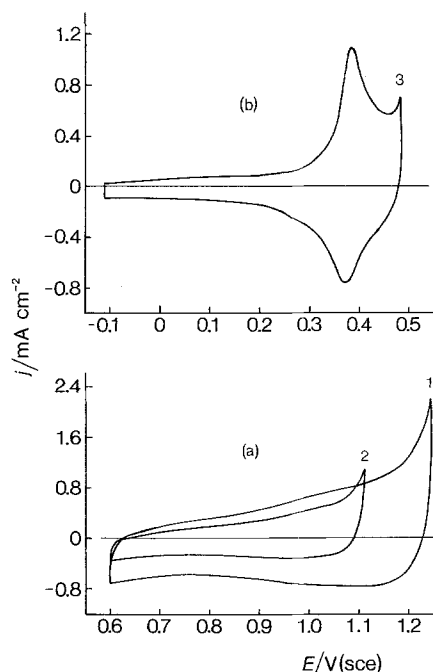


Fig. 1. Typical voltametric curves at  $20 \text{ mV s}^{-1}$  of  $\text{Co}_3\text{O}_4$  electrodes (with  $\text{RuO}_2$  interlayer) in (a) acidic and (b) basic solutions. 1.  $1 \text{ mol dm}^{-3} \text{ NaClO}_4 + 0.01 \text{ mol dm}^{-3} \text{ HClO}_4$ ; 2.  $5 \text{ mol dm}^{-3} \text{ NaCl} + 0.01 \text{ mol dm}^{-3} \text{ HCl}$ ; 3.  $1 \text{ mol dm}^{-3} \text{ KOH}$ . Temperature of preparation: (a)  $230^\circ \text{C}$ ; (b)  $300^\circ \text{C}$ .

tials were also measured at variable pH between 1 and 3. No dependence of  $E$  on pH was observed in the low  $p_{\text{Cl}_2}$  range which indicates that no mixed potential is appreciably operative in these conditions. In the high  $p_{\text{Cl}_2}$  range small effects were observed at the lowest  $\text{Cl}^-$  concentrations.  $\text{Cl}_2$  hydrolysis may perhaps have some effect at

high  $\text{Cl}_2$  pressure and low  $\text{Cl}^-$  concentration. The (possible) dissolution of the oxide [14] plays, however, a minor role in the range of low  $\text{Cl}_2$  overpotential.

Measured potentials are systematically higher by *c.* 4 mV in the region where Nernstian response is observed than those calculated from tabulated  $E^0$  and  $a_{\text{Cl}^-}$  data [15], most of the difference being presumably related to the unknown value of the liquid junction potential. The highest difference in the region where deviation from the Nernst slope is observed does not exceed 8 mV. Therefore, in the analysis which follows, thermodynamic reversible behaviour will be assumed throughout between 1 and 3. No dependence of  $E$  on pH was observed which indicates that no mixed potential is operative in this pH range at  $\text{Co}_3\text{O}_4$  surfaces. The (possible) dissolution of the oxide [15] therefore plays a minor role in the range of low  $\text{Cl}_2$  overpotentials.

### 3.3. Kinetic measurements close to equilibrium

Fig. 3 shows a typical polarization resistance determination around the equilibrium potential. The reversibility and reproducibility are very satisfactory although small hysteresis effects can be occasionally observed. This may be due to a small drift of the solution pH if  $\text{Cl}_2$  hydrolysis is allowed to proceed for too long a time.

The apparent exchange current was derived from the slope of the straight lines such as that in Fig. 3:

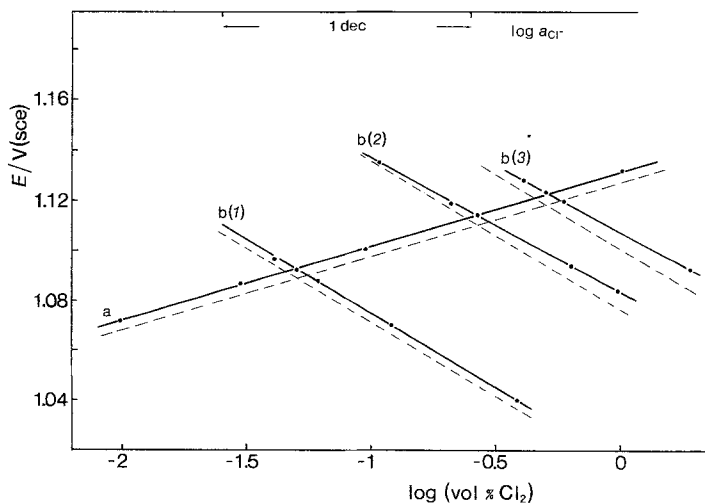


Fig. 2. Equilibrium potentials of  $\text{Co}_3\text{O}_4$  electrodes in  $\text{Cl}_2$  saturated solutions of  $\text{NaCl} + 0.01 \text{ mol dm}^{-3} \text{ HCl}$ : (a) at constant  $\text{NaCl}$  concentration ( $1 \text{ mol dm}^{-3}$ ) and variable  $\text{Cl}_2$  partial pressure; (b) at constant gaseous composition 1. 4.98, 2. 26.2, 3. 49.9 vol%  $\text{Cl}_2 + \text{N}_2$ , and variable  $\text{Cl}^-$  activity. Solid lines: experimental data. Dashed lines: calculated by the Nernst equation with  $E^0 = 1.358 \text{ V (NHE)}$  and  $E = 0.241 \text{ V (NHE)}$  for the saturated calomel electrode.

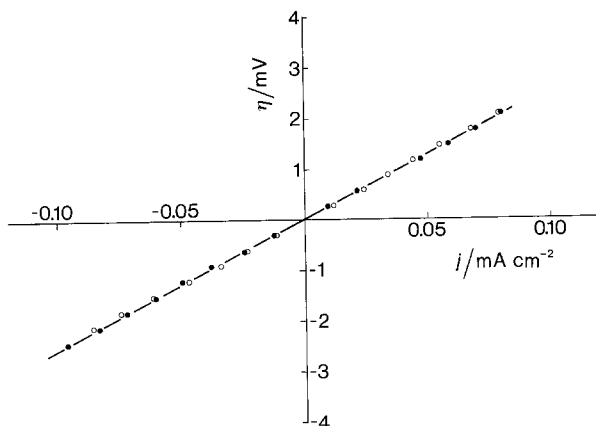


Fig. 3. Typical  $j$ - $\eta$  relationship around the equilibrium potential for a  $\text{Co}_3\text{O}_4$  electrode ( $260^\circ\text{C}$ , with  $\text{RuO}_2$  interlayer) in a  $1\text{ mol dm}^{-3}\text{ NaCl} + 0.01\text{ mol dm}^{-3}\text{ HCl}$  solution saturated with pure  $\text{Cl}_2$  gas. Different symbols indicate different runs ( $\circ$  - forward and  $\bullet$  - backward).

$$(j_0/\nu) = (RT/nF)(dj/d\eta) \quad (1)$$

Fig. 4 shows a typical plot of  $(j_0/\nu)$  as a function of  $\text{Cl}_2$  partial pressure ( $\text{Cl}_2$  is assumed to behave ideally). The dashed lines mark the slope equal to 0.5. Although for some electrodes, especially the more active ones (namely, those prepared at low calcination temperatures) the point for the lowest  $\text{Cl}_2$  pressure falls somewhat far from the straight line, the experimental data can be taken to conform to a linear dependence. Since:

$$(d \log j_0/d \log p_{\text{Cl}_2})_{\mu_{\text{Cl}^-}, T} = \alpha \quad (2)$$

it follows from Fig. 4 that the anodic transfer coefficient ( $\alpha$ ) is very close to 0.5.

With the aim of determining the cathodic

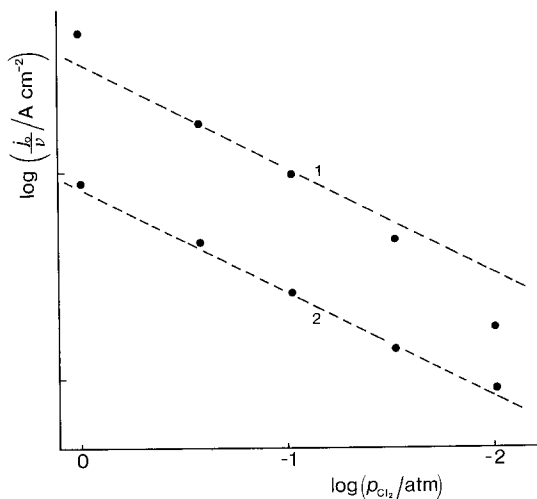
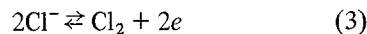


Fig. 4. Apparent exchange current obtained from plots such as Fig. 3 as a function of  $\text{Cl}_2$  partial pressure for two  $\text{Co}_3\text{O}_4$  electrodes. 1.  $260^\circ\text{C}$ , with  $\text{RuO}_2$  interlayer; 2.  $400^\circ\text{C}$ . (---) Relationship expected for  $\alpha = 0.5$ .

transfer coefficient independently, the apparent exchange current is plotted in Fig. 5 against the  $\text{Cl}^-$  activity at constant chlorine pressure. The striking feature of the resulting plot is not its nonlinearity but rather its negative slope throughout. Since the equilibrium potential is governed by the overall reaction:



as inferred from the Nernstian behaviour, the

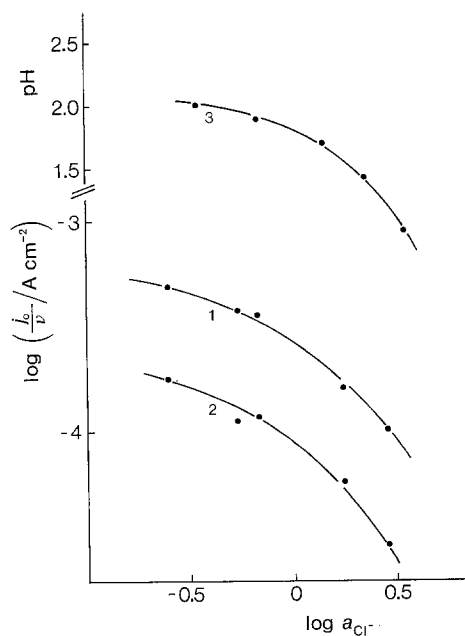


Fig. 5. Apparent exchange currents from plots such as Fig. 3 as a function of  $\text{Cl}^-$  activity in  $\text{NaCl} + 0.01\text{ mol dm}^{-3}\text{ HCl}$  solutions for two  $\text{Co}_3\text{O}_4$  electrodes. 1.  $260^\circ\text{C}$ ; 2.  $500^\circ\text{C}$ , with  $\text{RuO}_2$  interlayer. Curve 3 shows the variation of the actual pH of the solutions as a function of  $\text{NaCl}$  concentration.

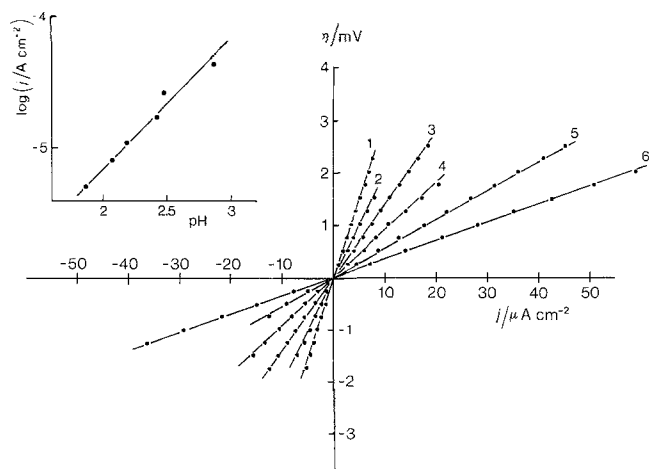


Fig. 6. Variation of the  $j$ - $\eta$  relationship around the equilibrium potential for a  $\text{Co}_3\text{O}_4$  electrode ( $400^\circ\text{C}$ ) in  $1\text{ mol dm}^{-3}$   $\text{NaCl}$  solutions at different pH saturated with 9.42 vol%  $\text{Cl}_2 + \text{N}_2$  gas. Equilibrium pH value: 1. 1.87; 2. 2.08; 3. 2.19; 4. 2.42; 5. 2.48; 6. 2.86. Inset: current density at  $\eta = 3\text{ mV}$  as a function of solution pH.

exchange current should depend on  $\text{Cl}^-$  activity as follows:

$$\left(\frac{d \log j_0}{d \log a_{\text{Cl}^-}}\right)_{T, \mu_{\text{Cl}_2}} = (x - 2\alpha) \quad (4)$$

where  $x$  is the reaction order with respect to  $\text{Cl}^-$ . Negative slopes can be obtained only if  $x$  is less than 1 which seems unlikely.

A clue to the understanding of this outcome can be found in the effect of pH. In principle, the pH should have nothing to do with the  $\text{Cl}_2$  equilibrium (provided the conditions are such as to minimize  $\text{Cl}_2$  hydrolysis effects, i.e.  $\text{pH} < 4-5$ ) [16]. However, the solution pH shifts with increasing  $\text{Cl}^-$  concentration as shown by Curve 3 in Fig. 5. This curve strikingly parallels the other two plots. Moreover, in a specific experiment, it was discovered that the apparent exchange current was markedly dependent on pH. This is clearly illustrated by Fig. 6. As shown in the inset, if the current at constant overpotential (recall that  $E_{\text{rev}}$  does not depend on pH) is plotted as a function of pH, a slope of about  $-1$  is found which means that  $\text{H}^+$  has a retarding effect on  $\text{Cl}_2$  evolution. This observation has never been reported before in the literature\*.

Since in Fig. 5 the exchange current appears to be entirely dominated by the pH shift,  $j_0$  is very likely to be independent of the  $\text{Cl}^-$  activity. Therefore  $x \approx 1$  in Equation 3 and the expression of the exchange current can be written as follows:

$$j_0 = nFk^0 a_{\text{Cl}_2}^\alpha a_{\text{Cl}^-}^{(1-2\alpha)} a_{\text{H}^+}^{-1} \quad (5)$$

where  $k^0$  is the standard rate constant. Therefore:

$$\begin{aligned} \left(\frac{d \log j_0}{d \log a_{\text{Cl}^-}}\right)_{\mu_{\text{Cl}_2}, T} \\ = (1 - 2\alpha) + \left(\frac{d \text{pH}}{d \log \text{Cl}^-}\right) \end{aligned} \quad (6)$$

Since in the explored concentration range, the second term on the left-hand side of Equation 6 is negative and  $(1 - 2\alpha) = 0$  with  $\alpha = 0.5$ , the slopes of the curves in Fig. 5 turn out to be negative. Thus the reaction of  $\text{Cl}_2$  at  $\text{Co}_3\text{O}_4$  anodes is thermodynamically independent of but kinetically dependent on the pH.

The effect of the 'electrochemically active surface area' is illustrated in Fig. 7. The points actually gather around a straight line of unit slope. The meaning of this result depends on the physical significance of  $q^*$ . Since  $q^*$  is largely determined by the anodic current peak prior to  $\text{O}_2$  evolution, the straight line in Fig. 7 suggests that  $\text{Cl}_2$  evolution takes place at the sites which are active in the adsorption of oxygenated species too. Should  $q^*$  measure the total surface area exposed to the solution and  $\text{Cl}_2$  evolution occur only at some specific sites whose surface concentration were an exponential function of the surface area, no linear correlation of unit slope would be observed. The same would be the case if the nature of the sites changed with surface concentration. Therefore, either (a) the surface concentration of active sites is directly proportional to the surface area and  $q^*$  measures the latter, or (b)  $q^*$  measures only the active surface area and no change in the nature of the surface sites occurs with the calcination temperature.

\* The effect of pH on  $\text{Cl}_2$  evolution was first reported by Krishtalik for  $\text{RuO}_2$  and  $\text{NiCo}_2\text{O}_4$  electrodes at a Symposium on Electrocatalysis in Neunkirchen, 14-16 September, 1983 (cf. Krishtalik *et al.* [17]).

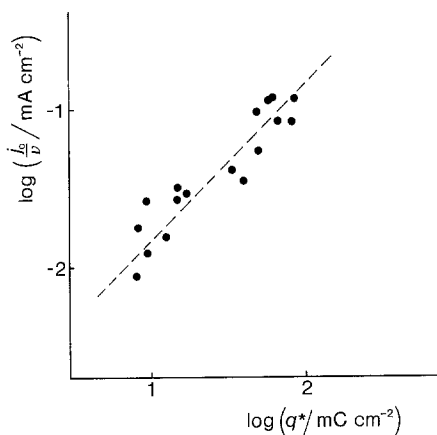


Fig. 7. Apparent exchange current from plots such as Fig. 3 as a function of the voltametric charge,  $q^*$ .  
----- Straight line of unit slope.

### 3.4. Kinetic measurements far from equilibrium

Fig. 8 illustrates the role played by the  $\text{RuO}_2$  interlayer. The experimental data have been corrected for the back reaction [18] and for the *IR drop in solution*. In fact, the latter correction was carried out by means of the current interruption technique using a Pt electrode in place of the  $\text{Co}_3\text{O}_4$  electrodes. This approach enables one to give evidence of any IR drop in the electrode. Fig. 8 shows that a single Tafel line of 0.040 V is observed up to  $0.1 \text{ A cm}^{-2}$  (higher current densities have not been explored but there is evidence that nothing different happens there) if a  $\text{RuO}_2$  interlayer is present between Ti and  $\text{Co}_3\text{O}_4$ . If  $\text{RuO}_2$  is not present,

deviations from the Tafel line are observed already at  $1 \text{ mA cm}^{-2}$ . This is clearly due to a  $\text{TiO}_2$  layer which, however thin, shows no miscibility with  $\text{Co}_3\text{O}_4$  [19] and therefore retains its largely insulating properties.

'True' exchange currents were obtained by back extrapolation of Tafel lines such as that in Fig. 8. By comparing 'apparent' and 'true' exchange currents the stoichiometric number could be obtained:

$$(j_0)_{\text{true}}/(j_0)_{\text{apparent}} = \nu \quad (7)$$

Fig. 9 shows a graphical analysis of  $\nu$  as a function of  $q^*$ . Out of 15 electrodes 11 gives a value of  $\nu$  between 1 and 1.1. The mean value is 1.18 which can reasonably be taken as 1 in view of the crucial inaccuracy of the extrapolation procedure (uncorrected *IR* drops tend to increase the resulting value of  $\nu$ ). It is to be noted that there is no significant systematic dependence of  $\nu$  on  $q^*$ .

In Fig. 10 the activity of  $\text{Co}_3\text{O}_4$  electrodes is compared with that of an  $\text{RuO}_2$  electrode [20]. Comparison is made with due attention to the value of  $q^*$ , but it is clear that the same physical significance cannot be attached unambiguously to the same value of  $q^*$  for the two oxides. Comparison shows that the Tafel slope is the same (0.040 V) but  $\text{Co}_3\text{O}_4$  electrodes are always less active even for higher  $q^*$  values. The results shown above warn that meaningful comparison is possible only if the solution pH is the same.

The Tafel slope is graphically analysed as a function of  $q^*$  in Fig. 11. Values derived from

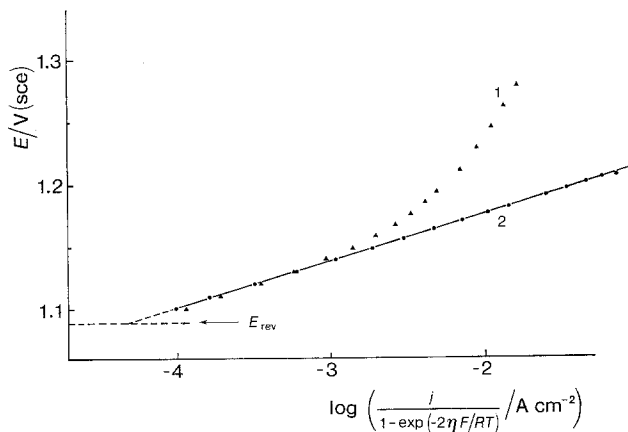


Fig. 8.  $\eta$ - $\log j$  relationship (corrected for the back reaction) for two  $\text{Co}_3\text{O}_4$  electrodes prepared at  $260^\circ \text{C}$ : 1. without  $\text{RuO}_2$  interlayer; 2. with  $\text{RuO}_2$  interlayer.  $1 \text{ mol dm}^{-3}$   $\text{NaCl}$  solution saturated with 4.98 vol%  $\text{Cl}_2 + \text{N}_2$  gas. Overpotentials corrected for the solution ohmic drop. — Tafel slope of 0.0395 V.

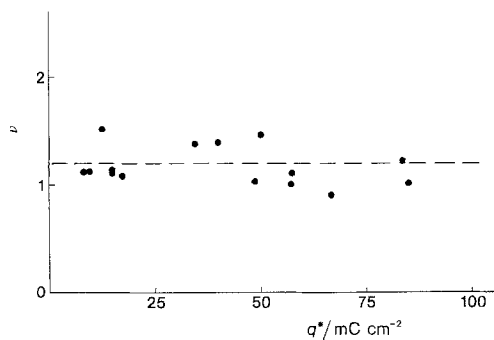


Fig. 9. Stoichiometric number for the chlorine evolution reaction, obtained from the ratio between the true exchange current extrapolated from plots such as Fig. 6 and the apparent exchange current from plots such as Fig. 3, as a function of the voltametric charge,  $q^*$ .

polarization data both in the absence and in the presence of  $\text{Cl}_2$  dissolved in solution are reported<sup>†</sup>. The most probable value is  $0.040 \pm 3$  mV and no systematic variation with  $q^*$  can be seen. Worthy of mention are the lower Tafel slope for the electrodes with very high value of  $q^*$ . The significance of lower Tafel slope values for very active electrodes has been recently illustrated by Losev [21]. Apparent overcorrections of the  $IR$  drop which should be in fact related to  $\text{Cl}_2$  diffusion [22] and saturation problems were actually observed in this work with the most active electrodes. An example is shown in Fig. 10.

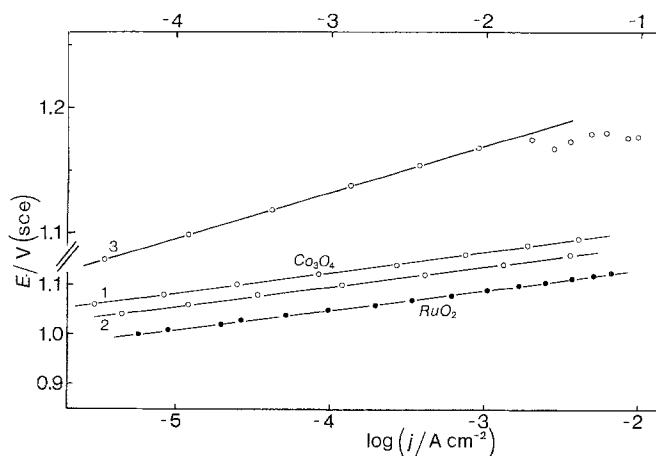


Fig. 10. Comparison of the activity of a Ti/RuO<sub>2</sub> electrode (300° C,  $q^* = c. 5$  mC cm<sup>-2</sup>) with the activity of two Co<sub>3</sub>O<sub>4</sub> electrodes for Cl<sub>2</sub> evolution from N<sub>2</sub> saturated 5 mol dm<sup>-3</sup> NaCl + 0.01 mol dm<sup>-3</sup> HCl solutions. 1. 400° C,  $q^* = c. 5$  mC cm<sup>-2</sup>; 2. 230° C, with a RuO<sub>2</sub> interlayer,  $q^* = c. 75$  mC cm<sup>-2</sup>. 3. As for line 2 but in the higher potential range. Potentials corrected for the solution ohmic drop. ——— - Tafel slopes of 0.00395 V.

<sup>†</sup> It is to be noted that Tafel lines in the absence and in the presence of  $\text{Cl}_2$  dissolved in solution match perfectly. Therefore, the reaction order with respect to  $\text{Cl}_2$  is zero.

### 3.5. Effect of electrode morphology

Fig. 12 illustrates the general relationship between the electrocatalytic activity and the calcination temperature used to prepare the Co<sub>3</sub>O<sub>4</sub> layers. The role of the RuO<sub>2</sub> interlayer does not appear to be crucial in this context. The decrease in activity as  $T$  increases parallels the observed decrease in the BET surface area [8]. The small rise in activity at the higher temperatures may be related to some underlayer effect (Co<sub>3</sub>O<sub>4</sub> on pure Ti does not work at 500° C owing to very large ohmic drop effects).

It has been suggested [6] that the activity of Co<sub>3</sub>O<sub>4</sub>, once corrected for surface roughness, still depends on the number of point defects in the lattice (metal vacancies balanced by Co<sup>3+</sup> in place of some Co<sup>2+</sup> sites). It is difficult in this work to disentangle the two effects if they are both present. It is however worth mentioning that the value of  $x$  in Co<sub>3-x</sub>O<sub>4</sub> is usually determined gravimetrically at the given temperature [23]. Co<sub>3</sub>O<sub>4</sub> can, however, release and take up oxygen again reversibly [24, 25] and this must be especially true at the surface. In another work [26], we have found that the point of zero charge of Co<sub>3</sub>O<sub>4</sub> does not depend on the calcination temperature. Should the surface stoichiometry depend on this parameter, the variable nature of the surface

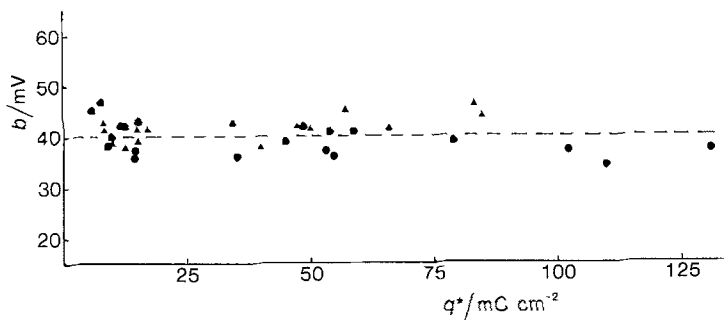


Fig. 11. Dependence of the Tafel slope for  $\text{Cl}_2$  evolution on the voltametric charge,  $q^*$ , of  $\text{Co}_3\text{O}_4$  electrodes. ● -  $\text{N}_2$  saturated  $5 \text{ mol dm}^{-3}$  NaCl solutions; ▲ -  $1 \text{ mol dm}^{-3}$  NaCl solutions saturated with 4.98 vol%  $\text{Cl}_2$ .

would show up through the point of zero charge. Therefore, this particular point deserves further careful study.

The effect of the electrode morphology shows up clearly in Fig. 13 where the electrocatalytic activity at two  $\text{Cl}^-$  concentrations is plotted as a function of  $q^*$ . While in Fig. 13a the experimental points are grouped around a straight line of unit slope, deviation from this behaviour is observed in solution at a lower  $\text{Cl}^-$  concentration. This outcome can be understood in terms of porosity of the active layer. The supply of  $\text{Cl}^-$  ions to the inner surface in pores is increasingly difficult as

the  $\text{Cl}^-$  concentration decreases. Under similar circumstances only part of the inner surface works, hence the electrocatalytic activity appears to decrease.

Porosity effects with  $\text{Co}_3\text{O}_4$  electrodes are, however, of minor importance. In concentrated brine they are not observed. Much more striking results have been reported [20, 27] for  $\text{RuO}_2$  electrodes. In that case porosity effects smooth down electrocatalytic activity differences even in  $5 \text{ mol dm}^{-3}$  NaCl solutions.

### 3.6. Activation energy

The activation energy,  $E^\ddagger$ , is a kinetic parameter

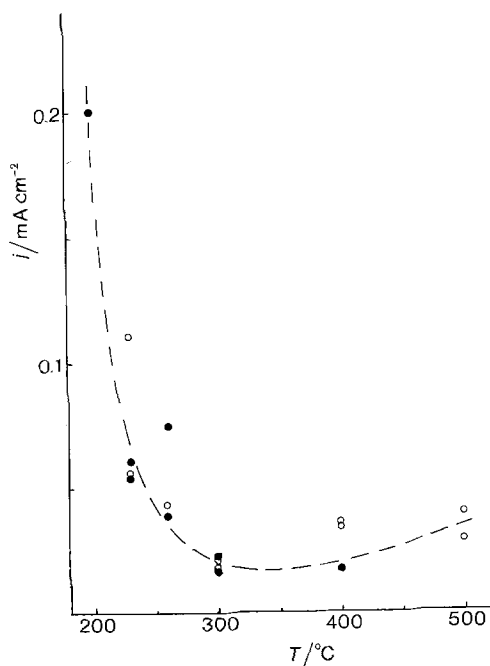


Fig. 12. Variation of the electrocatalytic activity of  $\text{Co}_3\text{O}_4$  electrodes for  $\text{Cl}_2$  evolution from  $\text{N}_2$  saturated  $4.5 \text{ mol dm}^{-3}$  NaCl solutions with the temperature of preparation. ● - without  $\text{RuO}_2$  interlayer; ○ - with  $\text{RuO}_2$  interlayer.  $E = 1.1 \text{ V (SCE)}$ .

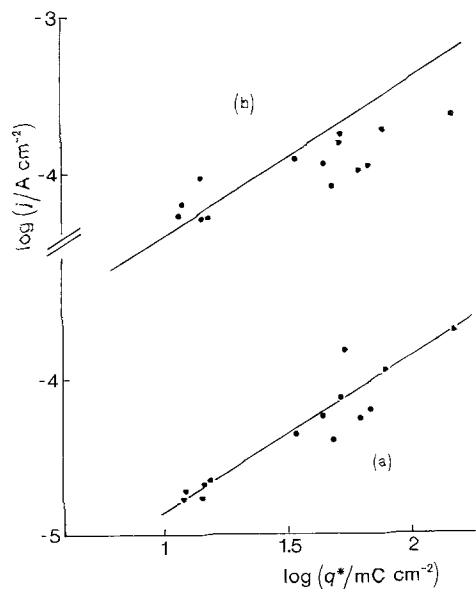


Fig. 13. Variation of the electrocatalytic activity of  $\text{Co}_3\text{O}_4$  electrodes for  $\text{Cl}_2$  evolution with the voltametric charge,  $q^*$ , in  $\text{N}_2$  saturated (a)  $4.5$  and (b)  $0.5 \text{ mol dm}^{-3}$  NaCl solutions.  $E = 1.1 \text{ V (SCE)}$ . — - straight line of unit slope.



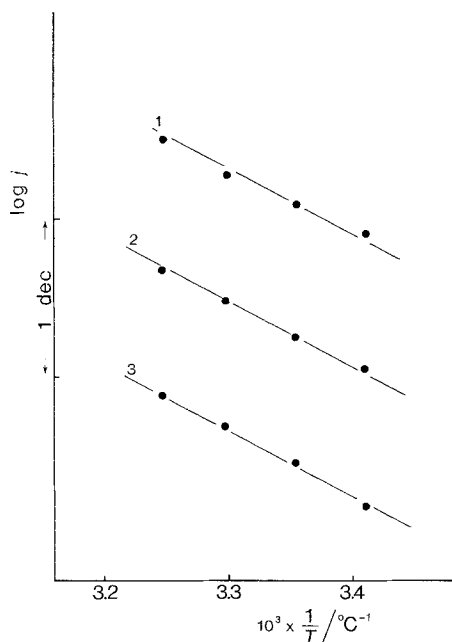


Fig. 14. Typical Arrhenius plots of the electrocatalytic activity for Cl<sub>2</sub> evolution as a function of reciprocal temperature for three Co<sub>3</sub>O<sub>4</sub> electrodes in N<sub>2</sub> saturated 5 mol dm<sup>-3</sup> NaCl solutions. 1. 260° C, with RuO<sub>2</sub> interlayer; 2. 300° C; 3. 500° C, with RuO<sub>2</sub> interlayer.  $E = 1.1$  V (SCE).

of difficult quantitative interpretation because the energetic state of adsorbed intermediates is usually not known.  $E^\ddagger$  is however very useful on a qualitative basis for comparison between different electrodes.

Fig. 14 shows a typical Arrhenius plot for the dependence of the activity of Co<sub>3</sub>O<sub>4</sub> electrodes in Cl<sub>2</sub> evolution on temperature. The derived  $E^\ddagger$  amounts to about  $75 \pm 4$  kJ mol<sup>-1</sup> and its depen-

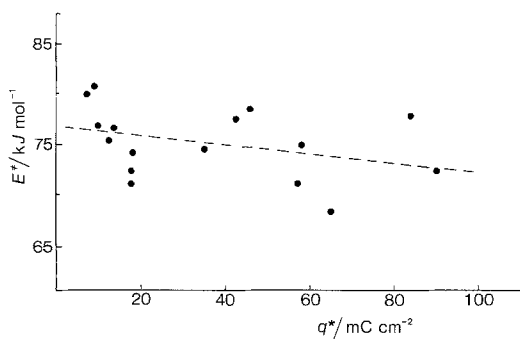


Fig. 15. Variation of the apparent activation energy for Cl<sub>2</sub> evolution on Co<sub>3</sub>O<sub>4</sub> electrodes with the voltametric charge,  $q^*$ . N<sub>2</sub> saturated 5 mol dm<sup>-3</sup> NaCl + 0.01 mol dm<sup>-3</sup> HCl solutions.  $E = 1.1$  V (SCE). ----- straight line calculated by the least squares method.

dence on  $q^*$  is shown in Fig. 15. If the points are analysed by the least squares method, some possible dependence on  $q^*$  shows up (see the dashed straight line). The total variation of  $q^*$  is c. 3 kJ mol<sup>-1</sup> over a  $q^*$  range of c. 90 mC cm<sup>-2</sup>. This amounts to about 4% of the total value of  $E^\ddagger$  and is probably not very significant. On the other hand, as seen in Fig. 11, Cl<sub>2</sub> diffusion problems may become appreciable as  $q^*$  increases. Therefore, the small decrease of  $E^\ddagger$  might be consistently understood in terms of a small diffusion component in the reaction rate.

### 3.7. Reaction orders

Since the Tafel slope of 0.040 V may be consistent with a number of different mechanisms, the reaction order becomes the crucial factor to discriminate between the various possibilities. Much of the discussion that has arisen in the literature [28–31] about the mechanism of Cl<sub>2</sub> evolution at RuO<sub>2</sub> electrodes has been in fact centred on the most probable value of the reaction order with respect to Cl<sup>-</sup>. In what follows, it is shown that a source of divergence between different authors is probably the unexpected and unpredictable effect of the solution pH.

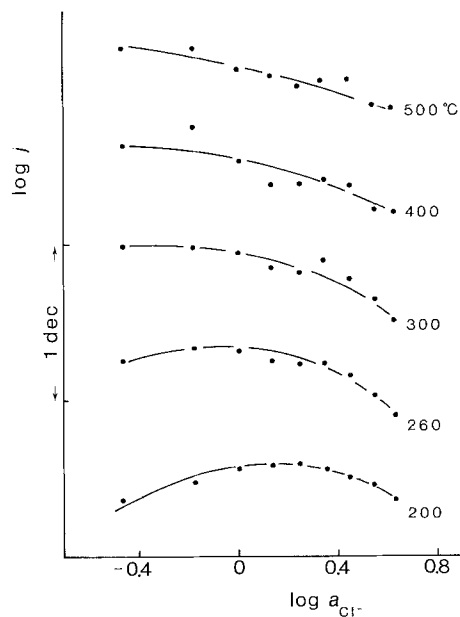


Fig. 16. Plot of the reaction rate for Cl<sub>2</sub> evolution at Co<sub>3</sub>O<sub>4</sub> electrodes against the Cl<sup>-</sup> activity at constant HCl concentration (0.01 mol dm<sup>-3</sup>).  $E = 1.1$  V (SCE).

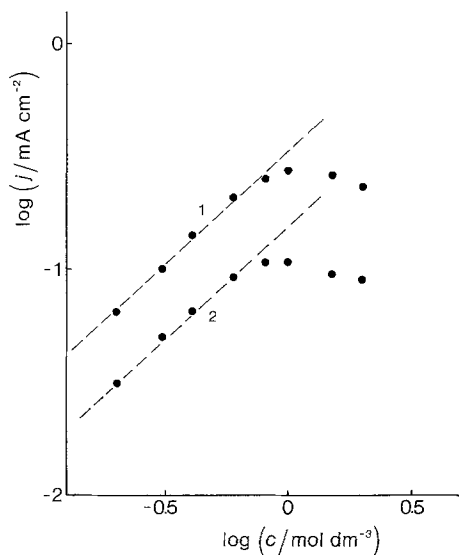


Fig. 17. Plot of the reaction rate for  $\text{Cl}_2$  evolution at two  $\text{Co}_3\text{O}_4$  electrodes against the  $\text{Cl}^-$  concentration in  $\text{NaCl} + 0.01 \text{ mol dm}^{-3} \text{ HCl} + 1 \text{ mol dm}^{-3} \text{ NaClO}_4$  solutions. 1.  $260^\circ \text{ C}$ ; 2.  $300^\circ \text{ C}$ , with  $\text{RuO}_2$  interlayer.  $E = 1.1 \text{ V}$  (saturated  $\text{NaCl}$ ). - - - - - straight line of unit slope.

Fig. 16 shows the variation of the reaction rate of  $\text{Cl}_2$  evolution with the  $\text{Cl}^-$  activity measured by simply changing the  $\text{Cl}^-$  concentration without any attention to the solution pH. The apparent reaction order is mainly negative, close to zero. For the most active electrodes it goes through a maximum at intermediate concentrations. Similar results for  $\text{RuO}_2$  electrodes were earlier interpreted [32] in terms of self-inhibition of the anodic reaction due to  $\text{Cl}^-$  specific adsorption.

If the determination of the reaction order is carried out with a constant large concentration of inert electrolyte, Fig. 17 shows that a reaction order of 1 tending to zero as the  $\text{Cl}^-$  concentration is increased is observed. Similar results for  $\text{RuO}_2$  electrodes were earlier interpreted [32] in terms of the screening effects of the electrode charge by the inert electrolyte and suppression of the  $\text{Cl}^-$  specific adsorption in the low  $\text{Cl}^-$  concentration range.

It is now clear that these results are due to the pH effects illustrated in Figs. 5 and 6. In particular, the smooth variation in shape of the curves in Fig. 16 is to be related to the combination of morphology and pH effects. More specifically, for the most active electrodes (low calcination temperature) the reaction rate is depressed at low  $\text{Cl}^-$  concentrations because of porosity effects

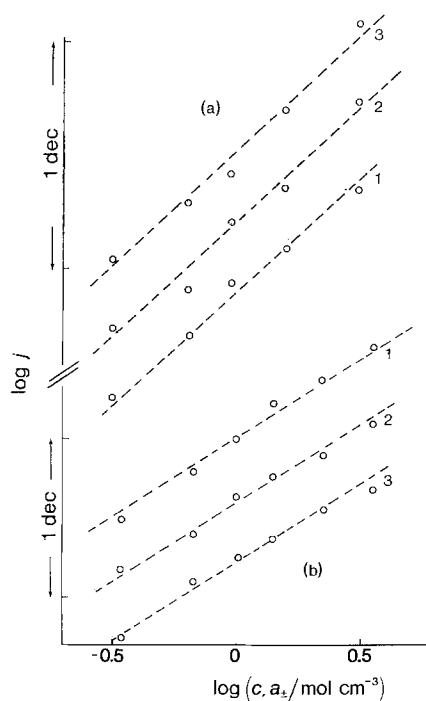


Fig. 18. Reaction rate for  $\text{Cl}_2$  evolution at  $\text{Co}_3\text{O}_4$  electrodes at variable  $\text{Cl}^-$  activity: (a) [ $E = 1.1 \text{ V (SCE)}$ ] and at variable  $\text{Cl}^-$  concentration in  $1 \text{ mol dm}^{-3} \text{ NaClO}_4$  solutions; (b) [ $E = 1.15 \text{ V (saturated NaCl)}$ ] at constant pH ( $c = 1$ ). - - - - - straight line of unit slope. Conditions of preparation: 1a.  $230^\circ \text{ C}$  with  $\text{RuO}_2$ ; 2a.  $400^\circ \text{ C}$ ; 3a.  $500^\circ \text{ C}$  with  $\text{RuO}_2$ ; 1b.  $230^\circ \text{ C}$ ; 2b.  $400^\circ \text{ C}$  with  $\text{RuO}_2$ ; 3b.  $500^\circ \text{ C}$  with  $\text{RuO}_2$ .

(cf. Fig. 13) and at high  $\text{Cl}^-$  concentrations because of pH effects. Therefore, the apparent reaction rate goes through a maximum. As the value of  $q^*$  decreases, then the porosity decreases. As a result, the variation of the reaction rate is dominated by pH effects over the  $\text{Cl}^-$  concentration range and it decreases monotonically with  $a_{\text{Cl}^-}$  (cf. the electrode prepared at  $500^\circ \text{ C}$ ).

The role of the solution pH is quantitatively illustrated in Figs. 18 and 19. The variation of the reaction rate with the activity of  $\text{Cl}^-$  in solution at constant pH is shown in Fig. 18, Curve a. The reaction order with respect to  $\text{Cl}^-$  is 1 beyond any reasonable doubt. Fig. 18, Curve b, shows that the same result is obtained in the presence of an inert electrolyte at high concentration. Fig. 19 shows that, at constant  $\text{Cl}^-$  concentration, the reaction rate is depressed by a decrease in the solution pH. The order of reaction with respect to  $\text{H}^+$  is therefore  $-1$ . The Tafel slope was not observed to depend on pH.

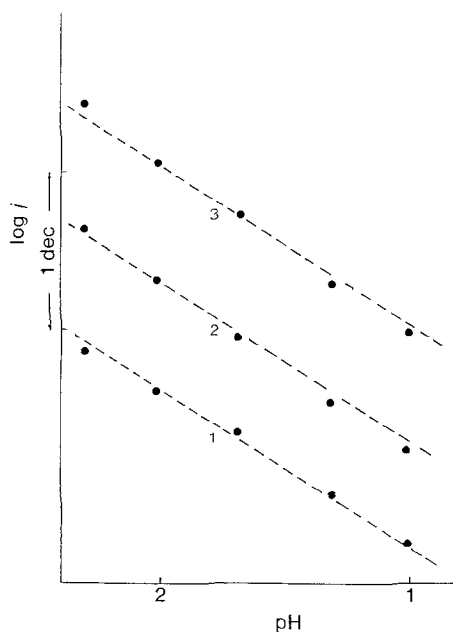


Fig. 19. Reaction rate at 1.1 V (SCE) for Cl<sub>2</sub> evolution at three Co<sub>3</sub>O<sub>4</sub> electrodes from 1 mol dm<sup>-3</sup> NaCl solutions as a function of the pH. ----- straight line of unit slope. 1. 230° C; 2. 300° C; 3. 400° C.

### 3.8. Reaction mechanism

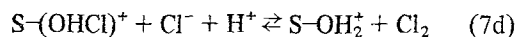
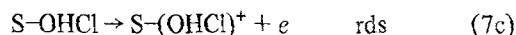
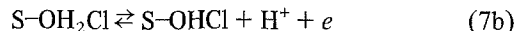
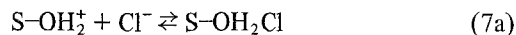
Table 1 summarizes the kinetic parameters of the anodic Cl<sub>2</sub> evolution reaction at Co<sub>3</sub>O<sub>4</sub> electrodes. These parameters do not depend on the procedure of preparation of the electrode. The standard rate constant is however strongly dependent on the temperature of calcination of the active layer. Results show that this dependence is related to the

Table 1. Summary of the kinetic parameters of the anodic evolution of chlorine at Co<sub>3</sub>O<sub>4</sub> electrodes

Parameter	Value
Reaction order ( $\eta = \text{const.}$ )	
Cl <sup>-</sup>	(1 - 2 $\alpha$ )
Cl <sub>2</sub>	$\alpha$
H <sup>+</sup>	- 1
Anodic transfer coefficient, $\alpha$	c. 0.5
Stoichiometric number, $\nu$	c. 1
Tafel slope	$RT/(1 + \alpha)F$
Reaction order ( $E = \text{const.}$ )	
Cl <sub>2</sub>	0
Cl <sup>-</sup>	1
H <sup>+</sup>	- 1
(Surface sites)	(1)
Activation energy, $E = 1.1$ V (SCE)	c. 75 kJ mol <sup>-1</sup>

variation with temperature in the surface concentration of active sites which appears to be proportional to the extension of the surface area. The order of reaction with respect to the active sites is therefore 1 and no extra electrocatalytic effects are produced by a change in the calcination temperature.

The Tafel slope of 0.040 V suggests that the second electron transfer is probably rate determining. However, the reaction order of 1 with respect to Cl<sup>-</sup> rules out the discharge of 2Cl<sup>-</sup> in the rate determining step and in the preceding steps. Moreover, the effect of the pH indicates that oxidation of hydroxylic species must precede the Cl<sup>-</sup> discharge. Therefore, electron transfer from Cl<sup>-</sup> is thought to take place at an oxidized site. The metal cation is probably inaccessible to direct discharge of Cl<sup>-</sup> because of coverage by water molecules and hydroxyl groups [13]. Since in the low pH range the surface of Co<sub>3</sub>O<sub>4</sub> is positively charged, a possible mechanism is the following:



where Reaction 7a expresses the electrostatic adsorption of negative ions onto positively charged sites.

The discharge of Cl<sup>-</sup> directly onto the metal cation is probably difficult because it would involve the displacement of a hydroxyl group by the chloride whose negative charge would then lead to true retarding effects. These have however been ruled out. Therefore, in the mechanism shown in Equations 7a-d the Cl<sup>-</sup> discharge is 'mediated' by the adsorbed OH group. This explains the role of the pH and also why no fractional reaction orders are observed, unlike the case of O<sub>2</sub> discharge [31, 33] which takes place at the bare cations of the oxide surface. The kinetic equation for the mechanism of Equations 7a-d is the following:

$$\eta = \ln 2Fk^0 - \frac{RT}{(1 + \alpha)F} \ln a_{\text{Cl}^-} + \frac{RT}{(1 + \alpha)F} \ln j + \frac{RT}{(1 + \alpha)F} \ln a_{\text{H}^+} \quad (8)$$

Table 2. Chronology of voltametric charge ( $q^*$ ) determination runs

Run	Description of the experiments
1	Fresh electrodes (After)
2	O <sub>2</sub> evolution from KOH solution (Tafel line)
3	O <sub>2</sub> evolution: reaction order and activation energy Cl <sub>2</sub> reaction: reaction resistance at different $a_{\text{Cl}^-}$ and different $p_{\text{Cl}_2}$ (About one year interruption)
4	Cl <sub>2</sub> evolution from 5 mol dm <sup>-3</sup> NaCl (Tafel line)
5	Cl <sub>2</sub> evolution: reaction order (Cl <sup>-</sup> )
6	Cl <sub>2</sub> evolution from 1 mol dm <sup>-3</sup> NaCl (Tafel line) Activation energy in 5 mol dm <sup>-3</sup> NaCl
7	Cl <sub>2</sub> evolution: reaction resistance in 1 mol dm <sup>-3</sup> NaCl
8	Cl <sub>2</sub> evolution from 1 mol dm <sup>-3</sup> NaCl with Cl <sub>2</sub> (Tafel line)
9	Voltametric curves far from O <sub>2</sub> evolution in a narrow potential range to investigate surface area
10	Cl <sub>2</sub> evolution: reaction order (Cl <sup>-</sup> ) in the presence of inert electrolyte

The involvement of oxygenated species in the mechanism of Cl<sub>2</sub> evolution has been suggested several times for RuO<sub>2</sub> electrodes [27–29, 34]. However, the kinetic role of protons has never been pointed out except in the very recent work of Krishtalik *et al.* [17]. In particular, Harrison, Caldwell and White [35] have suggested that HClO may be involved as an electroactive species,

but they failed to observe any pH effect in Cl<sub>2</sub> evolution at TiO<sub>2</sub> + RuO<sub>2</sub> electrodes [28]. Therefore, they have proposed [28] that water discharge follows (and does not precede) the Cl<sup>-</sup> discharge, which is physically much more difficult to rationalize.

### 3.9. External surface stability

While no specific study of the anodic wear under high current density was carried out, the stability of the electrode was monitored by measuring the voltametric charge  $q^*$  before and after each set of experiments. The chronological sequence of the experiments is detailed in Table 2.

Fig. 20 displays the variation of  $q^*$  in the course of the experiments. The vertical dashed line marks an interruption in the use of these electrodes for about one year. The general trend of  $q^*$  is to increase with use. This suggests that the surface probably undergoes a continuous wear (however small) that results in roughening. The increase in  $q^*$  is, however, not indefinite. After some runs,  $q^*$  decreases sharply or even collapses. This is presumably due to some mechanical 'polishing' of the surface resulting in removal of the smaller particles.

The general trend is also observed to depend on the temperature of preparation of the electrode, which points to the role of morphology. Fig. 21 shows the average behaviour of  $q^*$  as a function of the calcination temperature. Since an increase in  $q^*$  is paralleled by an increase in electrocatalytic activity, Fig. 21 shows that this

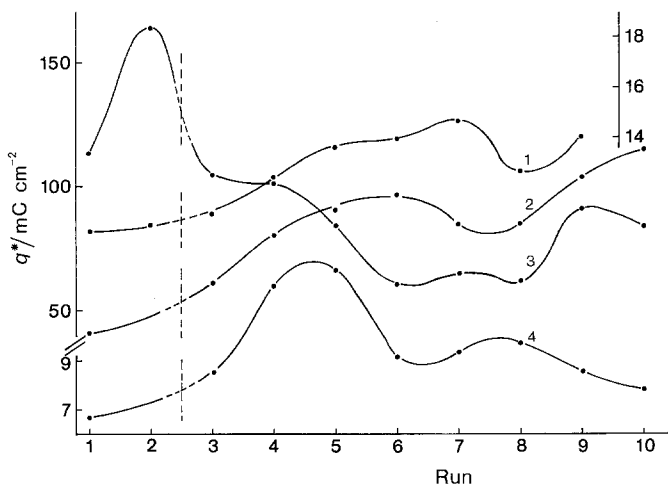


Fig. 20. Modification of the voltametric charge of Co<sub>3</sub>O<sub>4</sub> electrodes in the course of the experiments, as described in Table 1. 1. 300° C, with RuO<sub>2</sub> interlayer; 2. 230° C, with RuO<sub>2</sub> interlayer; 3. 200° C; 4. 400° C. For the vertical dashed line, see text.

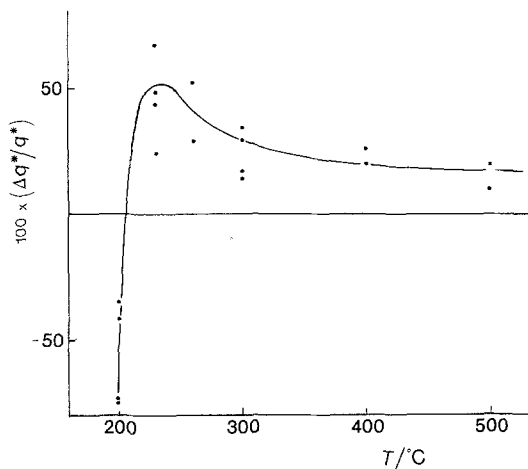


Fig. 21. Relative variation of the voltametric charge of  $\text{Co}_3\text{O}_4$  electrodes between Point 2 and Point 3 in Fig. 20, as a function of the temperature of preparation.

beneficial effect is maximum at temperatures around  $250^\circ\text{C}$ . At  $200^\circ\text{C}$  the trend is towards a sharp decrease of  $q^*$  which indicates that the active layer is very disperse and poorly adherent. In the high temperature range,  $q^*$  tends to a moderate increase with a substantial stability of the surface morphology.

### 3.10. Inner interface stability

The value of  $q^*$  is not sensitive to modifications at the support–active layer interface unless a blocking effect occurs. Evidence for a deterioration of the ohmic contact between Ti and the overlayer is provided by the potential difference between the anodic and cathodic peaks of the voltametric curve in KOH. With fresh electrodes with a  $\text{RuO}_2$  interlayer, the two peaks fall almost at the same potential. Fig. 22 shows that after the electrodes have been used in experiments the two peaks shift further apart. This might be related to the increased irreversibility of the adsorption–desorption reaction of oxygenated species but the distortion of the voltametric curve, and the features which will be illustrated below, lead us to think that the apparent decoupling of the peaks is probably related to the growth of an insulating layer at the Ti–oxide interface.

Fig. 23 illustrates the dependence of the peak separation on the calcination temperature and the presence or absence of the  $\text{RuO}_2$  interlayer. Fresh

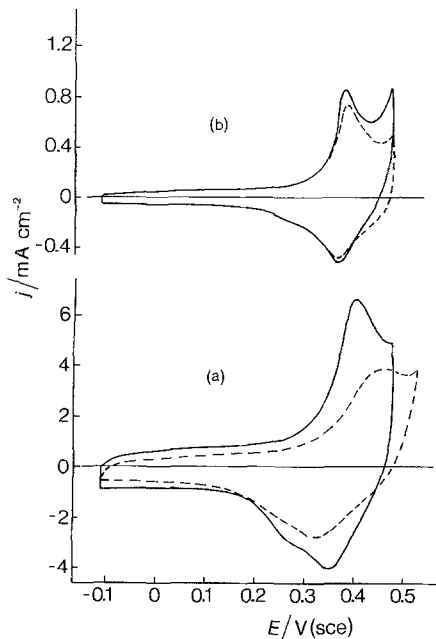


Fig. 22. Comparison of voltametric curves between  $\text{Co}_3\text{O}_4$  electrodes — with and — without  $\text{RuO}_2$  interlayer in correspondence to Point 9 in Fig. 20: (a)  $230^\circ\text{C}$ ; (b)  $400^\circ\text{C}$ .

electrodes with  $\text{RuO}_2$  interlayer show no peak separation down to *c.*  $260^\circ\text{C}$ . At lower temperatures some peak separation appears also with  $\text{RuO}_2$ . This may be due to the fact that at the lowest temperature the oxide layer is constituted by poorly adherent (see above), extremely fine particles. Thus, the electrocatalyst does not protect the underlying Ti surface from contact

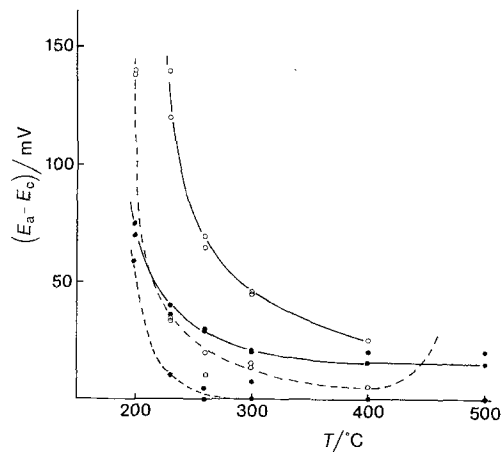


Fig. 23. Difference between anodic and cathodic peak potentials — — — — — for fresh  $\text{Co}_3\text{O}_4$  and — — — — — for electrodes in correspondence to Point 4 in Fig. 20. Electrodes ● — with and ○ — without  $\text{RuO}_2$  interlayer.

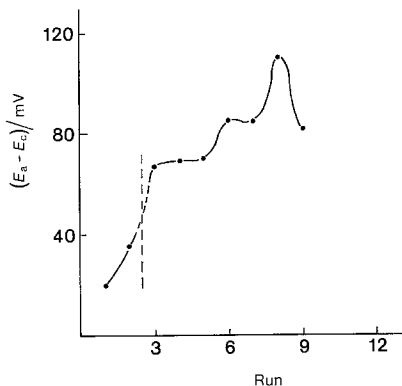


Fig. 24. Variation in the course of experiments, as described in Table 1, of the difference between anodic and cathodic peak potentials for a  $\text{Co}_3\text{O}_4$  electrode prepared at  $260^\circ\text{C}$  without  $\text{RuO}_2$  interlayer.

with the solution in the cell and the oxygenated atmosphere outside the cell. Moreover, lattice constituents are presumably very mobile in the presence of a large number of defects. In the absence of the  $\text{RuO}_2$  interlayer, fresh electrodes exhibit peak separation at any calcination temperature. After some use, the peak separation increases. The increase is minimum for electrodes with the  $\text{RuO}_2$  interlayer prepared at temperatures between  $300$  and  $500^\circ\text{C}$ .

Fig. 24 illustrates, for one specific electrode, the variation of the peak separation in the course of the experiments. It is interesting that polarization during  $\text{O}_2$  evolution or  $\text{Cl}_2$  evolution from diluted brines enhances the peak separation. Polarization in concentrated brine, on the contrary, does not produce any appreciable change in  $q^*$ . Therefore, the occurrence of water or  $\text{OH}^-$  discharge seems to be responsible for the change in  $q^*$ . Since  $\text{O}_2$  evolution leads to some ordering in the  $\text{Co}_3\text{O}_4$  lattice with shift of the composition towards stoichiometry [36], the peak separation might also be related to modifications in the structure of the oxide surfaces. The decrease in  $q^*$  in Fig. 24 in fact took place after some experiments where no oxygen was evolved and the potential was mainly kept far from the anodic limit. In this case, however, the peak separation should be visible also with fresh electrodes and should be a function of the calcination temperature, since stoichiometry increases as the temperature is raised.

The alternative possibility is that only during

oxygen evolution can oxygenated species reach the Ti surface where the insulating layer can grow and this is easier with defective, poorly crystalline, finely dispersed electrocatalysts. On the other hand, the peak separation with fresh electrodes without  $\text{RuO}_2$  is very likely to be due to the presence of the  $\text{TiO}_2$  insulating layer. Thus, the two mechanisms might be both operative, but the latter should largely prevail.

#### 4. Conclusions

$\text{Co}_3\text{O}_4$  exhibits an interesting activity for the anodic evolution of  $\text{Cl}_2$ . Although  $\text{RuO}_2$  is intrinsically more active, the difference is small enough to make the replacement of the precious metal oxide economically favourable. However, long-term performances have not been investigated specifically.

The activity of  $\text{Co}_3\text{O}_4$  electrodes depends on the temperature of their preparation. It increases exponentially with decreasing temperature below  $300^\circ\text{C}$  but the stability of the active layer becomes poorer. At temperatures higher than  $400^\circ\text{C}$  the oxide layer is very stable but its activity is low because of excessive crystallization and sintering.

Problems arise at the oxide-Ti interface. During the calcination, a  $\text{TiO}_2$  film is formed. Its effect can be minimized by interposing a thin layer of  $\text{RuO}_2$ . Without this layer, no electrode can be prepared at temperatures higher than  $400^\circ\text{C}$ . In the lower temperature range the insulating layer may form during anodic polarization because the active oxide is poorly crystalline and non-protective. Low-temperature layers deteriorate mechanically rather easily upon use.

Anodic  $\text{Cl}_2$  evolution at  $\text{Co}_3\text{O}_4$  electrodes is kinetically controlled by the interfacial transfer of the second electron. The first electron is, however, not exchanged with a  $\text{Cl}^-$  ion but with an adsorbed oxygenated species which thus releases a proton. This step is responsible for the observed pH dependence of the reaction rate which is thermodynamically unpredictable. In particular, the anodic reaction rate is depressed by an increase in the acidity of the solution. This unexpected kinetic feature of  $\text{Cl}_2$  evolution at oxide electrodes is very likely to be the origin of the discrepancies between the results of different authors and for

the consequent long debate about the mechanism of the anodic reaction.

### Acknowledgements

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### Note added in proof

With this paper already submitted for publication, Dr R. G. Erenburg has drawn the authors' attention to a paper in Dvoynoi Sloi i Adsorbtsiyana Tverdykh Elektrodakh, Vol 6, Tartus. Gos. Univ., 1981, pp. 382–5 (in Russian) where a mechanism similar to that proposed in this paper was first postulated.

### References

- [1] D. L. Caldwell and M. J. Hazelrigg, in 'Modern Chlorine Alkali Technology', (edited by M. O. Coulter) Ellis Horwood, Chichester (1980) pp. 121–135.
- [2] A. Tvarusko, 34th ISE Meeting, Erlangen, 19–23 September 1983. Extended Abstract III–7.
- [3] M. B. Kononov, V. I. Bystrov and V. L. Kubasov, *Elektrokhim.* **12** (1976) 1266.
- [4] R. A. Agapova and G. N. Kokhanov, *ibid.* **12** (1976) 1649.
- [5] D. M. Shub, M. F. Reznik, V. V. Shamaginov, E. N. Lubnin, N. V. Kozlova and V. N. Lomova, *ibid.* **19** (1983) 502.
- [6] V. V. Shalaginov, D. M. Shub, N. V. Kozlova and V. N. Lomova, *ibid.* **19** (1983) 537.
- [7] M. R. Tarasevich and B. N. Efremov, in 'Electrodes of Conductive Metallic Oxides'. Part A (edited by S. Trasatti) Elsevier, Amsterdam (1980) pp. 221–259.
- [8] R. Garavaglia, C. M. Mari, S. Trasatti and C. De Asmundis, *Surf. Technol.* **19** (1983) 197.
- [9] G. Lodi, E. Sivieri, A. De Battisti and S. Trasatti, *J. Appl. Electrochem.* **8** (1978) 135.
- [10] A. Carugati and S. Trasatti, in preparation.
- [11] C. M. Mari, R. Garavaglia, A. Carugati and S. Trasatti, 31st ISE Meeting, Venice, 1980. Extended Abstracts, p. 49.
- [12] B. N. Efremov and M. R. Tarasevich, *Elektrokhim.* **17** (1981) 1672.
- [13] A. Daggetti, G. Lodi and S. Trasatti, *Mater. Chem. Phys.* **8** (1983) 1.
- [14] R. Parsons, 'Handbook of Electrochemical Constants', Butterworths, London (1959).
- [15] D. M. Shub, A. N. Chemodanov and V. V. Shalaginov, *Elektrokhim.* **14** (1978) 595.
- [16] M. Spasojevic, N. Krstajic and M. Jaksic, *Surf. Technol.* **21** (1984) 19.
- [17] L. I. Krishtalik, R. G. Erenburg, D. V. Kokoulina and R. I. Mostkova, 34th ISE Meeting, Erlangen, 19–23 September 1983. Extended Abstract III–6.
- [18] B. V. Tilak, *J. Electrochem. Soc.* **126** (1979) 1343.
- [19] M. Valigi and D. Gazzoli, in 'Solid State Chemistry 1982', Elsevier, Amsterdam (1983) pp. 197–200.
- [20] S. Ardizzzone, A. Carugati, G. Lodi and S. Trasatti, *J. Electrochem. Soc.* **129** (1982) 1689.
- [21] V. V. Losev, *Elektrokhim.* **17** (1981) 733.
- [22] L. J. J. Janssen, G. J. Visser and E. Barendrecht, *Electrochim. Acta* **28** (1983) 155.
- [23] V. V. Shalaginov, I. D. Belova, Y. E. Roginskaya and D. M. Shub, *Elektrokhim.* **14** (1978) 1708.
- [24] W. K. Rudlof and E. S. Freeman, Proceedings of the 7th International Conference on Thermal Analysis **1** (1982) 667.
- [25] I. D. Belova, V. V. Shalaginov, B. S. Galyamov, Y. E. Roginskaya and D. M. Shub, *Zh. Neorg. Khim.* **23** (1978) 286.
- [26] S. Trasatti, *Electrochim. Acta* **29** (1984) 1503.
- [27] L. D. Burke and J. F. O'Neill, *J. Electroanal. Chem.* **101** (1979) 341.
- [28] D. A. Denton, J. A. Harrison and R. I. Knowles, *Electrochim. Acta* **24** (1979) 521.
- [29] T. Arikado, C. Iwakura and H. Tamura, *ibid.* **23** (1978) 9.
- [29] L. J. J. Janssen, L. M. C. Starmans, J. C. Visser and E. Barendrecht, *ibid.* **22** (1977) 1093.
- [31] L. I. Krishtalik, *ibid.* **26** (1981) 329.
- [32] R. G. Erenburg, L. I. Krishtalik and I. P. Yarosheskaya, *Elektrokhim.* **11** (1975) 1072.
- [33] A. Carugati, G. Lodi and S. Trasatti, *Mater. Chem.* **6** (1981) 255.
- [34] J. Augustynski, L. Balsenc and J. Hinden, *J. Electrochem. Soc.* **125** (1978) 1093.
- [35] J. A. Harrison, D. L. Caldwell and R. E. White, *Electrochim. Acta* **28** (1983) 1561.
- [36] B. N. Efremov, G. I. Zakharkin, S. R. Zhukov and M. R. Tarasevich, *Elektrokhim.* **14** (1978) 937.